# PDE and Boundary-Value Problems Winter Term 2014/2015 

## Lecture 3

Universität des Saarlandes
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## Purpose of Lesson

- To show how parabolic PDEs are used to model heat-flow and diffusion-type problems. To discuss the physical meaning of different terms (such as $u_{t}, u_{x}, u_{x x}$, and $u$ ) and present a few examples of parabolic equations.
- To give an intuitive feeling for parabolic-type problems.
- To show how heat-flow and diffusion-type problems can give rise to a variety of boundary conditions and to introduce the important concept of flux.


## Purpose of Lesson (continued)

- To discuss first of three important types of BCs:
(1) temperature specified on the boundary.

Chapter 2. Parabolic (Diffusion)-Type Problems.
We introduce a simple physical problem and show how it can be described by means of a mathematical model (model involves PDEs).

Then we complicate the problem and show how new PDEs can describe the new situations.

## Remark

Today we will not derive or solve PDEs. It will be done later.

A simple heat-flow experiment
Suppose we have the following simple experiment that we break into steps:

1. We start with a reasonable long (say $L=2 \mathrm{~m}$ ) rod 2 cm in diameter. The heat can flow in and out of the rod at the end, but not across the lateral boundary.
2. Next, we place this rod in an enviroment whose temperature is fixed at $T_{0}=10^{\circ} \mathrm{C}$ for a sufficiently long time. The temperature of the entire rod comes to a steady state temperature similar to the enviroment.
3. We take the rod out of the enviroment at the time that we call $t=0$ and attach two temperature elements to the end of the rod. These elements keep the ends at specific temperature $T_{1}=0^{\circ} \mathrm{C}$ and $T_{2}=50^{\circ} \mathrm{C}$.
4. Now we monitor the temperature profile of the rod on some type of display.

The mathematical model of the heat-flow experiment
The description of our heat-transfer problem requires three types of equations
(1) The PDE describing the physical phenomenon of heat flow.
(2) The boundary conditions describing the physical nature of our problem on the boundaries
(3) The initial conditions describing the physical phenomenon at the start of the experiment.

The heat equation
The basic equation of one-dimensional heat flow is the relationship

$$
\begin{equation*}
u_{t}=\alpha^{2} u_{x x}, \quad 0<x<L, \quad 0<t<\infty \tag{3.1}
\end{equation*}
$$

which relates the quantities
$u_{t}=$ the rate of change in temperature w.r.t. time
and
$u_{x x}=$ the concavity of the temperature profile $u(x, t)$.

## Remarks

- $u_{x x}$ compares the temperature at one point to the temperature at neighboring points.
- Equation (3.1) will be derived later from the basic conservation of heat equation.
- Eq. (3.1) says that the temperature $u(x, t)$ at some point $x$ and at some moment $t$ is increasing ( $u_{t}>0$ ) or decreasing ( $u_{t}<0$ ) according to whether $u_{x x}$ is positive or negative.
- The proportionality constant $\alpha^{2}$ is a property of the material.

How $u_{x x}$ can be interpreted to measure heat flow?
We approximate $u_{x x}$ by the difference quotient

$$
\begin{aligned}
u_{x x}(x, t) & \cong \frac{1}{(\Delta x)^{2}}[u(x+\Delta x, t)-2 u(x, t)+u(x-\Delta x, t)] \\
& =\frac{2}{(\Delta x)^{2}}\left[\frac{u(x+\Delta x, t)+u(x-\Delta x, t)}{2}-u(x, t)\right] .
\end{aligned}
$$

There is the following interpretation of $u_{x x}$ :

- If $u(x, t)<$ average of the two neighboring temperatures, then $u_{x x}>0$ (the net flow of the heat into $x$ is positive).
- If $u(x, t)=$ average of the two neighboring temperatures, then $u_{x x}=0$ (the net flow of the heat into $x$ is zero).
- If $u(x, t)>$ average of the two neighboring temperatures, then $u_{x x}<0$ (the net flow of the heat into $x$ is negative).


## Boundary conditions

All physical problems have boundaries of some kind, so we must describe mathematically what goes on there in order to adequately describe the problem.

Boundary conditions in our experiment:

$$
\left\{\begin{array}{l}
u(0, t)=T_{1}  \tag{3.2}\\
u(L, t)=T_{2}
\end{array} \quad 0<t<\infty\right.
$$

## Remark

Temperature $u$ was fixed for all time at $T_{1}$ and $T_{2}$ at the two ends $x=0$ and $x=L$.

## Initial conditions

All physical problems must start from some value of time (generally called $t=0$ ), so we must specify the physical apparatus at this time.

Initial conditions in our experiment

$$
\begin{equation*}
u(x, 0)=T_{0} \quad 0 \leqslant x \leqslant L \tag{3.3}
\end{equation*}
$$

## Remark

We started monitoring the rod temperature from the time the rod had achieved a constant temperature of $T_{0}$.

We have described the experiment.
Writing (3.1)-(3.3) together, we get an initial boundary value problem:

$$
\left\{\begin{array}{rlrl}
u_{t} & =\alpha^{2} u_{x x} & \quad 0<x<L, \quad 0<t<+\infty \\
u(0, t) & =T_{1} & & 0<t<+\infty \\
u(L, t) & =T_{2} & & 0<t<+\infty \\
u(x, 0) & =T_{0} & & 0 \leqslant x \leqslant L
\end{array}\right.
$$

Lateral heat loss proportional to the temperature difference
The equation

$$
u_{t}=\alpha^{2} u_{x x}-\beta\left(u-u_{0}\right) \quad \beta>0
$$

decribes heat flow in the rod with both
(1) diffusion $\alpha^{2} u_{x x}$ along the road and
(2) heat loss (or gain) across the lateral sides of the rod.

## Remark

Heat loss $\left(u>u_{0}\right)$ or gain $\left(u<u_{0}\right)$ is proportional to the difference between the temperature $u(x, t)$ of the rod and the surrounding medium $u_{0}$.

Internal heat source
The nonhomogeneous equation

$$
u_{t}=\alpha^{2} u_{x x}+f(x, t)
$$

correspond to the case where the rod is being supplied with an internal heat source (everywhere along the rod and for all time).

## Diffusion-convection equation

Suppose a pollutant is carried along in a stream moving with velocity $\nu$.

Let $u(x, t)$ be a concentration of the substance. The rate of change $u_{t}$ is measured by the diffusion-convection equation

$$
u_{t}=\alpha^{2} u_{x x}-\nu u_{x}
$$

where
$\alpha^{2} u_{x x}$ is the diffusion contribution
and
$-\nu u_{x}$ is the convection component.

Heat equation with variable coefficient
The heat equation

$$
u_{t}=\alpha^{2}(x) u_{x x}
$$

corresponds to a problem where the diffusion within the rod depends on $x$ (the material is nonhomogeneous).

## Boundary conditions for parabolic-type problems

Three basic types of boundary conditions can occur for heat-flow problems:
(1) $u=g(t)$;
(2) $\frac{\partial u}{\partial n}+\lambda u=g(t)$.
(3) $\frac{\partial u}{\partial n}=g(t)$.

Here $n$ ist the outward normal direction to the boundary.

Type 1 BC (Temperature specified on the boundary)

$$
\left\{\begin{array}{l}
u(0, t)=g_{1}(t) \\
u(L, t)=g_{2}(t)
\end{array}\right.
$$

(The same heat-flow experiment as in the beginning of the lecture)

## Remarks

- Problems with BCs of this kind are fairly common.
- It may be that the goal of the problem is to find the boundary temperatures (boundary control) $g_{1}(t)$ and $g_{2}(t)$ that will force the temperature to behave in a suitable manner.
- Similar types of BCs also apply to higher dimensional domains.

Type 1 BC (Temperature specified on the boundary)

## Example

In two dimensions we could imagine the problem of finding the temperature inside the circular disc (of radius $R$ ) when the boundary temperature is specified in polar coordinates to be

$$
u(R, \theta, t)=\cos t \sin \theta
$$

Type 1 BC (Temperature specified on the boundary)

$$
u(R, \theta, t)=\cos t \sin \theta
$$



Figure 1: Oscillating boundary temperature

